# RE-CORD



## Thermochemical Biofuel Conversion processes: overview and innovative approaches

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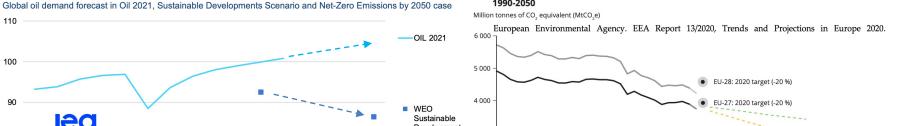


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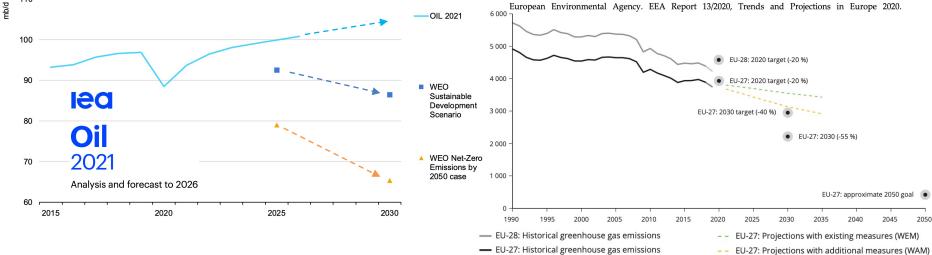
### Setting the scene: an unprecedent challenge

Oil demand off-course to meet sustainable development and net-zero targets



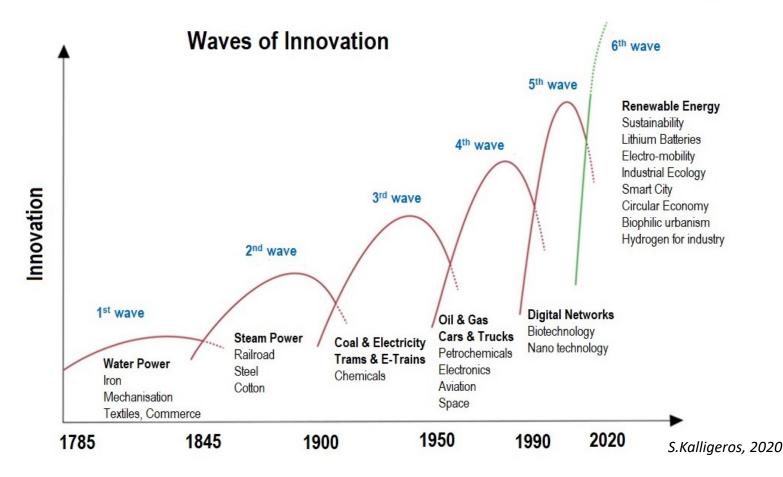
Greenhouse gas emission targets, trends, and Member States MMR projections in the EU,

1990-2050



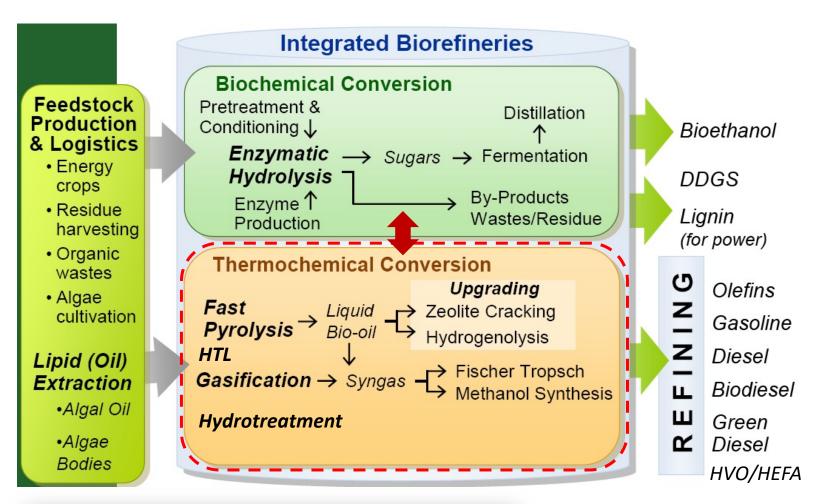






- Industrial scale-up & Policy making need to adapt to such fast changes
- > What is doable in the given timeframe? Do we meet the urgency?
- > Which socio-economic impacts?

# Biorefining & Thermochemical conversion



#### NREL Definition of Biorefinery

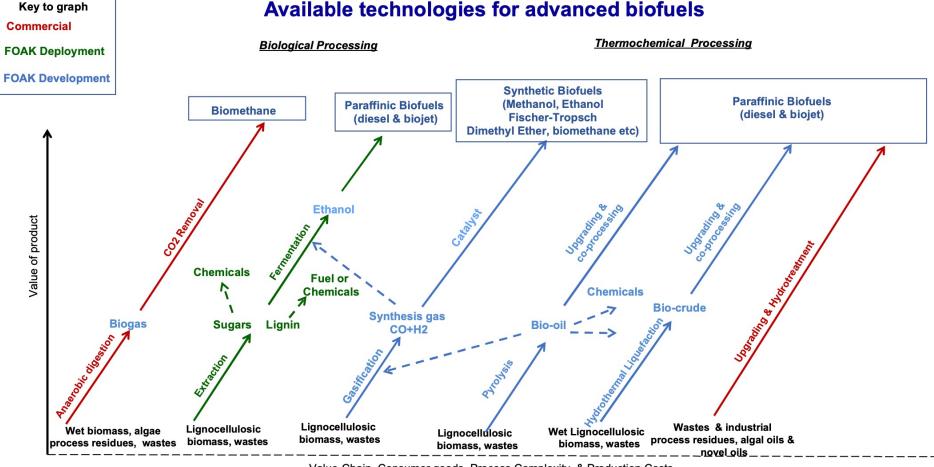
 "A facility that integrates biomass conversion processes and equipment to produce fuel, power and chemicals from biomass"

Source: elaborated from IEA-Bioenergy

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#### Available technologies for advanced biofuels

Value-Chain, Consumer goods, Process Complexity, & Production Costs

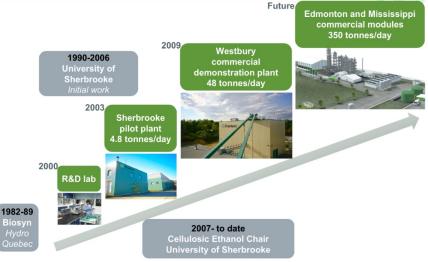
Adding value to biomass by processing to advanced biofuels and to biochemicals

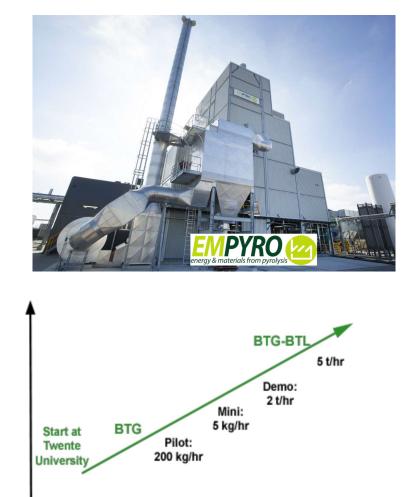




### From **Pilot** to Ind.**Demo** to **FOAK** (Mountain of Death) – Time to market





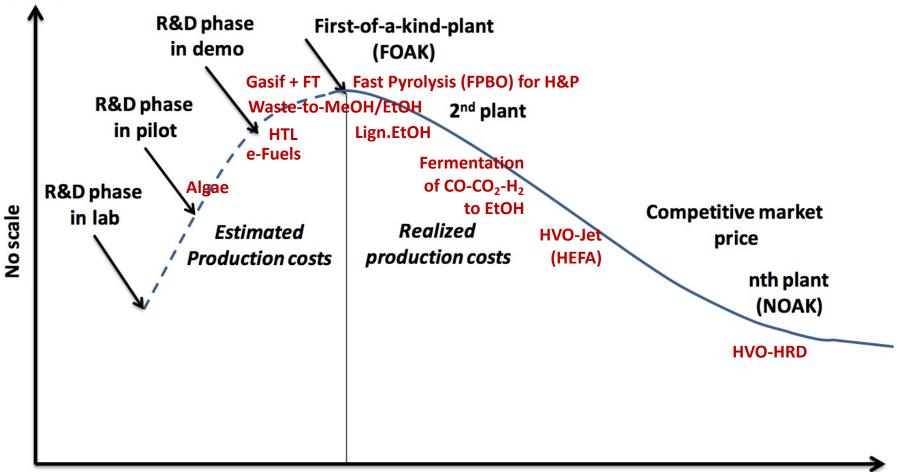




### **MOUNTAIN OF DEATH**



**Production cost** 



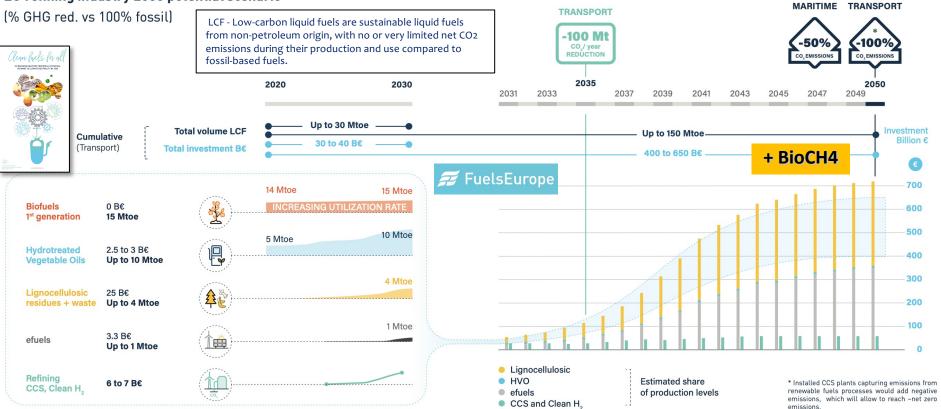
**Time** *Remark – estimates change with feedstock & application (CHP or Transport)* Author's elaboration from K.Maniatis / SGAB, 2017



### Refining industry forecasts



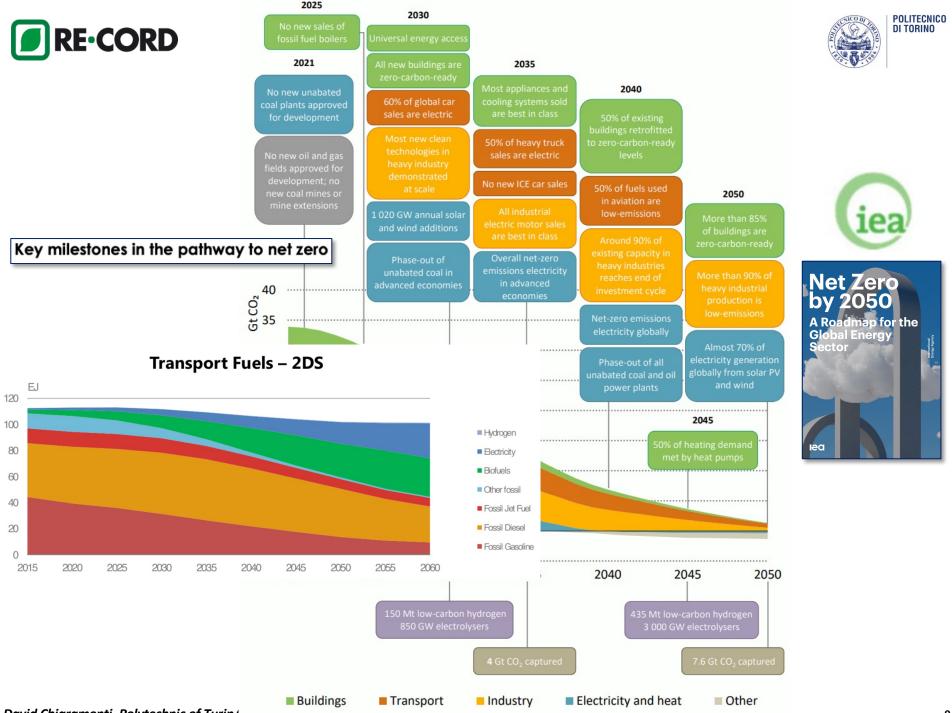
#### EU refining industry 2050 potential scenario



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**AVIATION &** 

ROAD

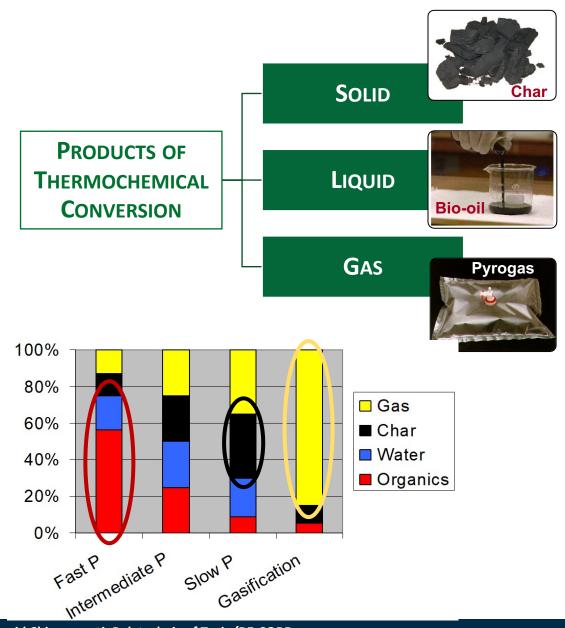


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9



### THERMOCHEMICAL CONVERSION PYROLYSIS / GASIFICATION 🕖



- **Pyrolysis** (Slow, Intermediate, Fast), **Gasification**
  - Fast Pyrolysis: some full-scale industrial plants. Focus on biocrude. Oil quality sensitive to Feedstock.
  - Slow Pyrolysis: very robust and mature technology. Many reactor types available at any size. A Multi-Feedstock technology focused on solids.
  - Gasification: well-developed and known. Scale vs feedstock and costs. Energy oriented, now shifting to Products. Conversion of gas into product as FT-fuels, MeOH/EtOH, etc. Also, FT products conversion in fossil refineries, Co-processing
- Pyrolysis, Gasification: DRY feed



Pressure [bar]



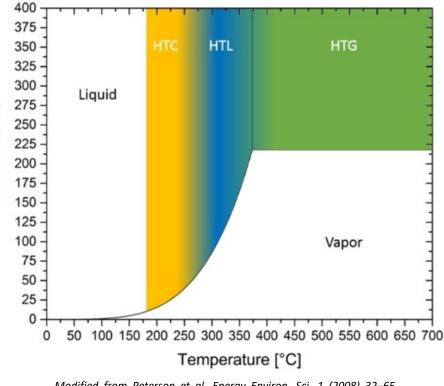
#### HydroThermal Processing routes

#### **HIGH T**

Higher T Super Crit. Conditions	HTG (HydroThermal Gasification)
High T <i>~Crit./Sup.</i> <i>Conditions</i> 280-370 °C	HTL (HydroThermal Liquefaction)
180-250 °C	HTC (HydroThermal Carbonisation)
180-250 °C 140-230 °C	HTC (HydroThermal Carbonisation)
	`
140-230 °C	LHW (Liquid How Water pre-treatment)

LOW T

✓ Hydrothermal Processing: WET feed



Modified from Peterson et al. Energy Environ. Sci. 1 (2008) 32–65. doi:10.1039/b810100k

### **HTL: Key needs and scale-up strategies**



- **<u>Residual/waste feedstocks</u>**: Genifuels (WWT), Steeper (Forest Residues, Sludges and MSW), ENI (OFMSW), Mura (end-of-life plastics)
- <u>**Co-Liquefaction:**</u> improved economics by enhanced feedstock availability
  - $\checkmark$  Synergistic effects for yield and biocrude quality reported
  - ✓ Wood + Algae, Sewage sludge + Lignocelluloses, Miscanthus + Polyurethane
  - ✓ Wheat straw + Manure, Sewage sludge + Swine manure (Mix with sewage sludge: No base catalyst, enhanced slurry pumpability)
- Water management: Recycle, Cat HTG (CH<sub>4</sub>-rich gas , high p and cat.deactivation), AD (proven, inhibition of MO, recovery of nutrients), LLE+APR (H<sub>2</sub> production)
- <u>Co-refining</u>: similar to FPBO (Stabilization + HDO + co-refining), but less oxygenated crude
  - ✓ Waste feedstock → Intensive hydrodenitrogenation (HDN) and hydrodesulphurization (HDS) are often needed to avoid catalyst deactivation
  - ✓ 3 EU projects considering HTL biocrude co-refining: 4refinery, Waste2Road, HyFlexFuel
- <u>Biocrude sCO<sub>2</sub> fractionation</u>: extraction yields above 50%, low water&metal content, avg mol.weight, density and viscosity, reduced acidity (shift to carboxylic instead of phenolic), moderate Oxygen content reduction. Longer HT catalyst life, lower hydrogen requirements, and less coking

### HTL: AQUEOUS PHASE MANAGEMENT

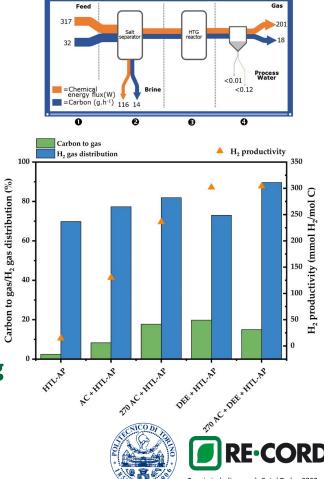


### > One of the main bottleneck for process scale-up. Options:

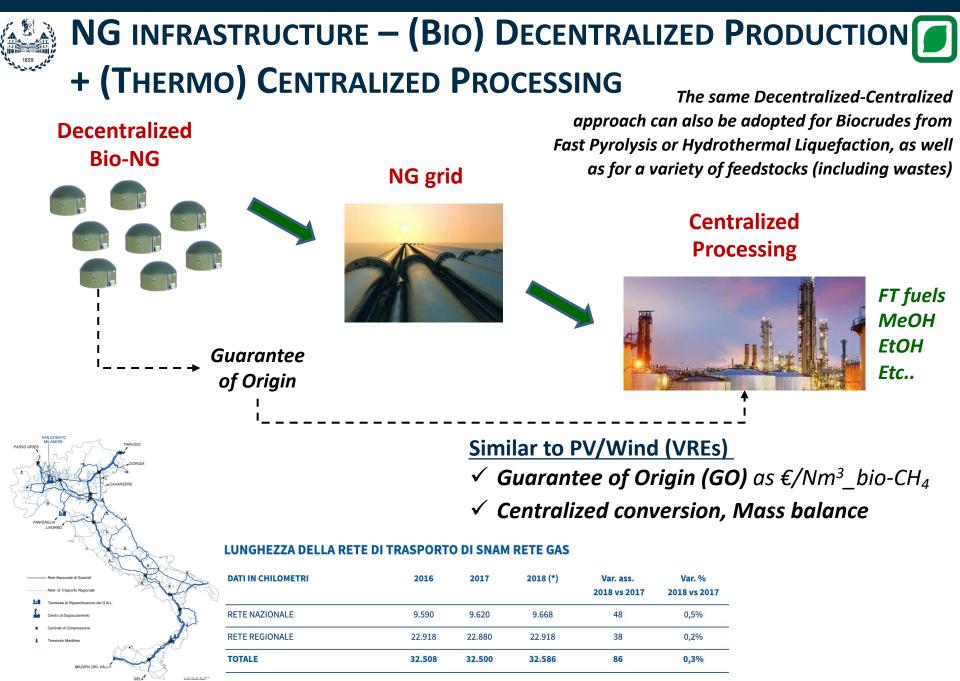
- Recycle
- Catalytic hydrothermal gasification (PNNL, PSI)
  - CH<sub>4</sub>-rich gas
  - High pressure equipment, catalyst deactivation
- Anaerobic digestion
  - Simple and well-proven technology
  - Inhibition of microorganisms
- Recovery of nutrients
- Liquid-liquid extraction + Aqueous phase reforming
  - H<sub>2</sub> production for biocrude upgrading
  - Catalyst deactivation





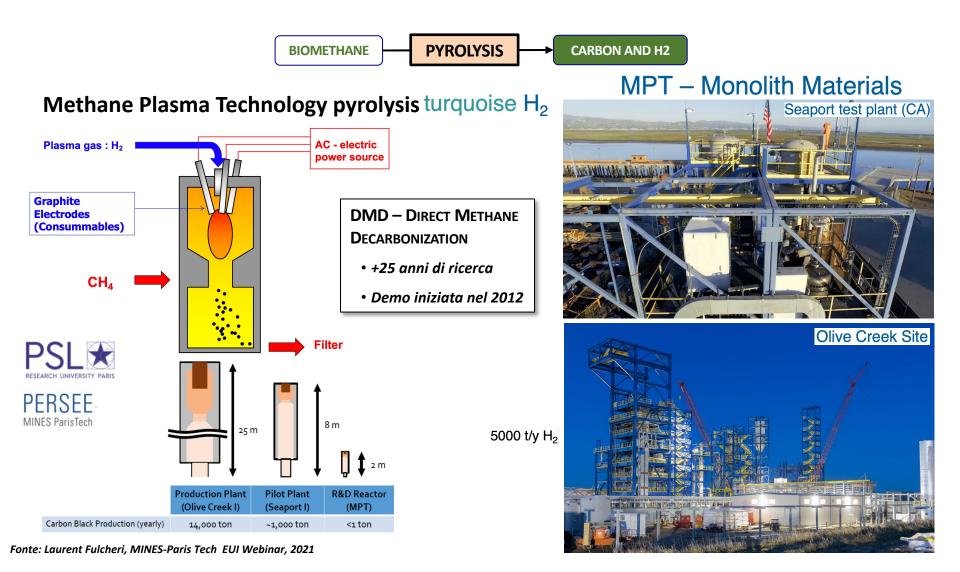


Zoppi et al., (in press), Catal Today 2020. doi:10.1016/j.cattod.2020.08.013



(\*) situazione ad ottobre 2018

### (BIO-)METHANE PYROLYSIS: GREY, BLUE, GREEN, TURQUOISE



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# **COMPARISON OF H<sub>2</sub> PRODUCTION ROUTES**



	kWh/kgH <sub>2</sub>	kWh/Nm <sup>3</sup> H <sub>2</sub>	kgCO <sub>2</sub> /kgH <sub>2</sub>	H <sub>2</sub> and Sustainability	Notes	
SMR	8.7	0.725	9.5-12	<b>Grey</b> H <sub>2</sub> <b>Green</b> H <sub>2</sub> <i>if from</i> <i>BioCH</i> <sub>4</sub>	Heavily exothermic reaction C released in gaseous form as CO <sub>2</sub> Low-C or at best Carbon Neutral only if combined with CCS Carbon Negative only if from combined with CCS and BioCH <sub>2</sub>	
Electrolysis	39.6 (Theoretical limit) 53-80 (Industrial)	-	-	<b>Green</b> <i>if from RES</i>	It requires Power (53 kWh/kg=63% eff) Power from RES to generate Green H <sub>2</sub>	
DMD-MPT	<b>10-20</b> (kWh <sub>e</sub> )	-	0	Turquoise	C separated as solid (C <sub>s</sub> ) It requires Power Low-C or at best Carbon Neutral Carbon Negative only if from BioCH <sub>2</sub>	
Bio-methane pyrolysis	11-15 (kWh <sub>e</sub> )	-	0	Green and Carbon Negative	C as solid (C <sub>s</sub> ) Elevated T (1300 °C) without catalyst The Catalyst can be bio-based It could be run without Power Demo needed. Costs to be confirmed and <i>f</i> ( <i>catalyst</i> ), but potentially low cost It generates C allowances	
H <sub>2</sub> via APR of Bio-residues	Low power demand (low TRL)	-	0	Green and Carbon Neutral or Negative	Variable yields depending on soluble organics C released in gaseous form as $CO_2$ . C negative if combined with CCS and biogenic $CO_2$ (in that case, C allowances are generated)	

Sources: Elaborations by PoliTO, Laurent Fulcheri (MINES-Paris Tech ) e Bernd Meyer e Roh Pin Lee (EUI Webinar), 2021; Parkinson et al., 2018

### AVIATION: THE CHALLENGE, AND THE NEED FOR AN EU CLEARINGHOUSE FOR NEW PROCESS ROUTES

- 142 Mt CAF at 2010 → 570-860 Mt at 2050 (International Aviation) + 400-600 % !!
- 100% CAF substitution (MAX scenario) 170 new biorefineries each year from 2020 to 2050 (15-60 \$B/y) - MAX would reduce CO<sub>2</sub> emission by 63% source: UN-ICAO

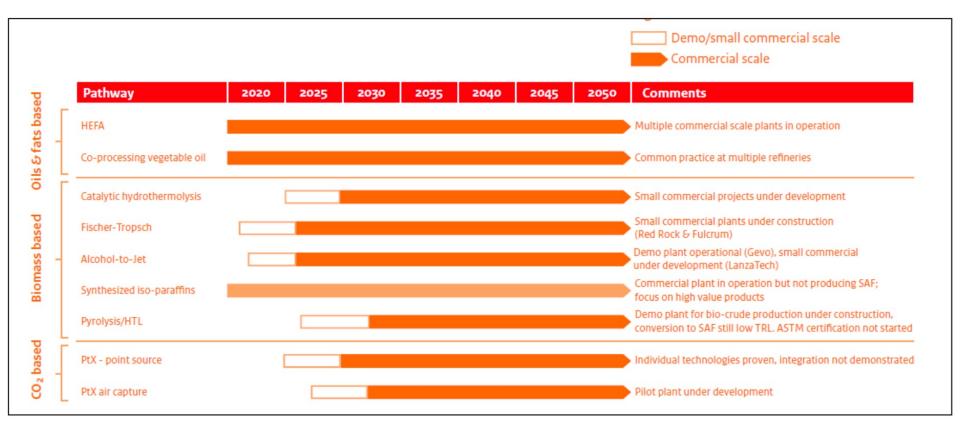


- Thermochemical processing can well target <u>SAF</u> (the most challenging fuel) and <u>Maritime</u>
- The US Clearinghouse supports ASTM certification path of new routes
- A similar Clearinghouse should be established in the EU



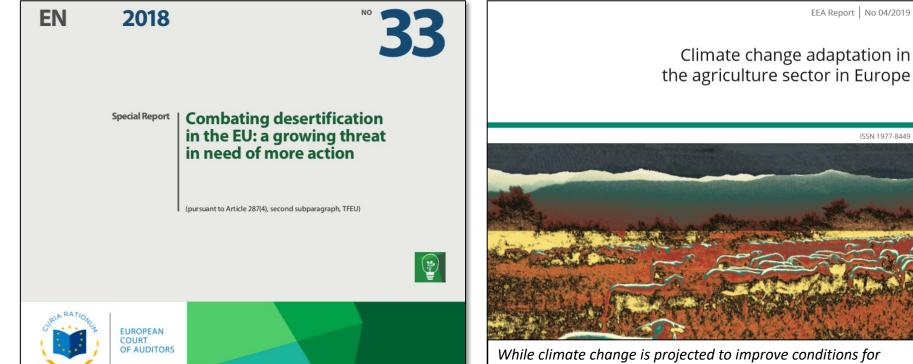
WDB Action programme





### SOIL: THE URGENT NEED TO TAKE ACTION

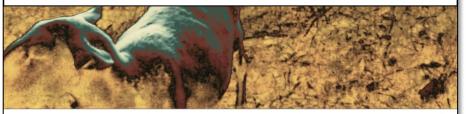




V. [..] **no EU-level strategy on desertification and land degradation**. Rather, there is a range of strategies, action plans and spending programmes, such as the Common Agricultural Policy, the EU Forest Strategy, or the EU strategy on adaptation to climate change, which are relevant to combating desertification, but which do not focus on it.

[...] we make recommendations to the Commission aimed at better understanding land degradation and desertification in the EU; assessing the need to enhance the EU legal framework for soil; and stepping up efforts towards delivering the **commitment** made by the EU and the Member States to achieve **land degradation neutrality in the EU by 2030.**  While climate change is projected to improve conditions for growing crops in parts of northern Europe, the **opposite** is true for crop productivity in **southern Europe**.

According to projections using a high-end emission scenario, yields of non-irrigated crops like wheat, corn and sugar beet are projected to decrease in southern Europe by up to 50 % by 2050.



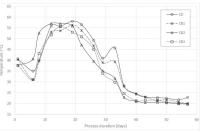


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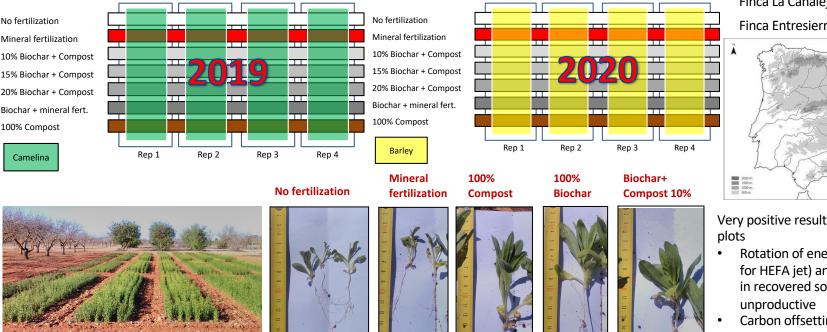
#### Biochar concentration in the final product: 14.9 - 19.8 - 22.8% w/w d.b.

(0)

Table 2 Initial windrows compositions

	U.M.	CD	CB1	CB2	CB3
Windrow	kg d.b.	160.6	156.5	153.0	149.6
Starting moisture	% w/w w.b.	61.6	60.0	59.2	58.3
Biochar content	kg w.b.	0.0	12.0	18.0	24.0
Biochar rate	% w/w d.b.	0.0	7.3	11.2	15.2
C/N index		36.3	40.4	42.7	45.2

### **Recovery of Low ILUC REDII marginal land through BIOCHAR and** co-composted biomass AD Digestate/biochar (COMBI) for HEFA

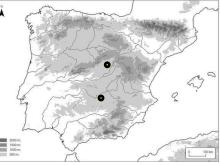


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Two sites in very dry and marginal areas in ES  $\rightarrow$ 

Finca La Canaleja (Madrid) – L1

Finca Entresierras (Ciudad Real) – L2



Very positive result in experimental

- Rotation of energy crops (Camelina for HEFA jet) and food/feed (barley) in recovered soil, otherwise
- Carbon offsetting
  - Improved resilience to Climate Change

### **CONCLUSIONS: CHALLENGES AND OPPORTUNITIES**



- Thermochemical conversion of biomass and waste is expected to play a leading role in the ecological transition
  - Multiple products can be obtained from biobased or circular carbon feedstocks
  - Scale-up and full replication beyond mountain of death post 2030?
- Focus on whole value-chain, not on fuel production step only
- •This chain will complement Biochemical, eFuels, RCF all options needed to meet the challenge
- Policy-driven markets
  - Framed in the Green Deal scheme, Fit-for-55 package and International (ICAO, IMO) regulations
  - Stable and doable policy needed to stimulate investments (large CAPEX)
- Way for EU economic recovery, supporting domestic chains



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# Thanks for your attention

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