

# concaawe



report no. 8/13

## Marine fuels and hydrogen sulphide



# Marine fuels and hydrogen sulphide

Prepared for the CONCAWE Fuels Quality and Emissions Management Group by its  
Marine Fuels Ad Hoc Group (reporting to FE/STF-24):

N. Elliott (Chair)  
F-J. Antunez Martel  
A. Bonini  
Ø. Buhaug  
F. Chevallier  
B. Heyberger  
H. Hovius  
L. Jansen  
V. Pocek  
A. P. Ramos  
S. Sasloglou  
K. Seppälä  
K. Steernberg  
R. Terschek  
M. Vermeire

K. D. Rose (Science Executive)

Reproduction permitted with due acknowledgement

© CONCAWE  
Brussels  
October 2013

## ABSTRACT

The safe handling of petroleum cargoes and refined products that may contain hydrogen sulphide (H<sub>2</sub>S) is an important issue for the marine and inland fuel industries. Attention has refocused recently on H<sub>2</sub>S due to the revision of the ISO 8217:2012 [1] specification for marine fuels which limited the maximum content of H<sub>2</sub>S in the liquid fuel to 2.00 mg H<sub>2</sub>S/kg fuel (2.00 ppmw).

This report summarizes issues associated with the presence of H<sub>2</sub>S in residual marine fuels including:

- Sources of H<sub>2</sub>S in petroleum products;
- Exposure levels for H<sub>2</sub>S in the vapour phase and the effects of exposure;
- Relationship between the H<sub>2</sub>S concentration in liquid fuel and in the vapour phase;
- Measurement methods for H<sub>2</sub>S in marine fuel and in the vapour phase;
- Interpretation of results and guidance on maximum H<sub>2</sub>S levels; and
- Guidelines for the safe handling of liquid petroleum products that may contain H<sub>2</sub>S.

Importantly, the report reinforces the need for safe handling procedures, training, and personnel protection when transferring or storing fuels that may contain H<sub>2</sub>S, rather than relying only on a measured H<sub>2</sub>S level in the liquid product.

## KEYWORDS

Marine fuel, residual marine fuel, residual fuel oil, marine distillate fuel, hydrogen sulphide

## INTERNET

This report is available as an Adobe pdf file on the CONCAWE website ([www.concawe.org](http://www.concawe.org)).

### NOTE

*Considerable efforts have been made to assure the accuracy and reliability of the information contained in this publication. However, neither CONCAWE nor any company participating in CONCAWE can accept liability for any loss, damage or injury whatsoever resulting from the use of this information.*

*This report does not necessarily represent the views of any company participating in CONCAWE.*

<b>CONTENTS</b>		<b>Page</b>
<b>SUMMARY</b>		<b>IV</b>
<b>1.</b>	<b>BACKGROUND</b>	<b>1</b>
<b>2.</b>	<b>SOURCES OF HYDROGEN SULPHIDE</b>	<b>2</b>
<b>3.</b>	<b>EFFECTS AND PROPERTIES OF H<sub>2</sub>S</b>	<b>4</b>
3.1.	OCCUPATIONAL EXPOSURE LIMITS FOR H <sub>2</sub> S IN THE VAPOUR PHASE	5
<b>4.</b>	<b>MEASUREMENTS OF H<sub>2</sub>S</b>	<b>6</b>
4.1.	MEASUREMENTS OF H <sub>2</sub> S IN THE LIQUID PHASE	6
4.2.	SAMPLING AND HANDLING CONSIDERATIONS	7
4.3.	MEASUREMENTS OF H <sub>2</sub> S IN THE VAPOUR PHASE	8
<b>5.</b>	<b>ISO 8217 GUIDANCE ON H<sub>2</sub>S LEVELS IN THE LIQUID PHASE</b>	<b>9</b>
<b>6.</b>	<b>PRODUCT HANDLING AND SAFETY PRECAUTIONS</b>	<b>10</b>
<b>7.</b>	<b>ACRONYMS</b>	<b>12</b>
<b>8.</b>	<b>ACKNOWLEDGMENTS</b>	<b>13</b>
<b>9.</b>	<b>REFERENCES</b>	<b>14</b>

## SUMMARY

The safe handling of petroleum cargoes and refined products that may contain hydrogen sulphide (H<sub>2</sub>S) is an important issue for the marine and inland fuel industries. Attention has refocused recently on H<sub>2</sub>S due to the revision of the ISO 8217:2012 [1] specification for marine fuels which limited the maximum content of H<sub>2</sub>S in the liquid fuel to 2.00 mg H<sub>2</sub>S/kg fuel (2.00 ppmw).

To raise awareness of the industry's experience with the safe handling of marine fuels, this report reviews issues associated with the presence and measurement of H<sub>2</sub>S in liquid fuels and the importance of safe handling procedures to limit personnel exposure to H<sub>2</sub>S.

At vapour concentrations well below 1 ppmv, H<sub>2</sub>S has the distinctive smell of rotten eggs which provides an early warning to personnel. At moderate vapour concentrations from 50 to 100 ppmv, H<sub>2</sub>S causes a marked sensory irritation, a temporary loss of sensitivity to H<sub>2</sub>S smell (transitory olfactory fatigue), headaches and dizziness. Exposure to H<sub>2</sub>S in the vapour phase may cause unconsciousness at concentrations higher than about 300 ppmv and death at concentrations higher than about 700 ppmv.

Hydrogen sulphide (H<sub>2</sub>S) is naturally present in crude oils and can be formed during the refining process and in storage tanks downstream of the refinery. Residual marine fuels and marine distillate fuels can contain H<sub>2</sub>S at various concentrations in the liquid phase. The H<sub>2</sub>S concentration in the liquid phase will depend on the crude oil, the specific refining processes (such as visbreaking or thermal cracking) used to produce the residual marine fuel, and the conditions under which the fuel is stored after production. H<sub>2</sub>S in the liquid phase of a petroleum product can evolve into the available vapour space of the product's storage tank. The relationship between liquid and vapour phase H<sub>2</sub>S concentrations is difficult to predict, however, because the vapour phase concentration depends on a number of fuel- and storage-related factors.

Although marine distillate fuels do not typically contain enough H<sub>2</sub>S in the liquid phase to cause safety concerns, higher liquid-phase levels of H<sub>2</sub>S can be found which can result in higher than expected vapour phase concentrations of H<sub>2</sub>S under some circumstances.

The oil and shipping industries routinely handle cargoes (such as sour crude oils and high-sulphur process streams) that contain much higher liquid phase H<sub>2</sub>S levels than those that are typically found in residual marine fuels. Robust safety procedures, based on industry experience and reinforced by personnel training, have been successful in providing a high degree of protection to personnel working in the vicinity of these cargoes. Proper safety, handling, and emergency procedures are the primary control measure to prevent H<sub>2</sub>S-related safety incidents and to ensure that personnel are not exposed to high vapour phase H<sub>2</sub>S levels (see Section 6).

In order to provide even greater protection to personnel, a maximum liquid phase H<sub>2</sub>S limit of 2.00 mg H<sub>2</sub>S/kg fuel, as measured by test method IP 570 [2], was added to the ISO 8217 specification in 2010 for marine fuels, effective August 2012.

The Standard Method IP 570 is the recommended test method for measuring H<sub>2</sub>S in the liquid phase of fuel oils. This method provides an approximation of the total H<sub>2</sub>S which can be evolved into the vapour phase from a given sample of fuel oil. Other methods, such as IP 399<sup>1</sup> [3] may also be used to analyse liquid fuels as long as users

---

<sup>1</sup> The Energy Institute's IP Test Panel is no longer technically revising IP 399.

satisfy themselves that the alternative method gives reliable results compared to IP 570. However, in cases of dispute, IP 570 is the referee test method.

For measuring H<sub>2</sub>S in field applications, some methods can be used to estimate vapour phase H<sub>2</sub>S concentration, such as the use of stain detector tubes or electronic monitors. Although these methods are reliable and suited for monitoring H<sub>2</sub>S concentrations in the workplace, the conditions under which the vapour phase sample is taken can introduce variability in the measured H<sub>2</sub>S levels in the vapour phase, resulting in abnormally low results and a false sense of security that the fuel contains a low level of liquid phase H<sub>2</sub>S.

This new liquid phase H<sub>2</sub>S limit in ISO 8217 is intended to provide an additional margin of safety by reducing the risk that personnel are exposed to levels of H<sub>2</sub>S vapour that can cause sudden and severe health effects. This limit alone, however, should not be considered a completely safe level and does not eliminate the risk that H<sub>2</sub>S vapour will evolve to very high concentrations in enclosed spaces. It also does not replace the need for proper procedures, control measures, and appropriate personal protection for all operations in which personnel could be exposed to H<sub>2</sub>S in the vapour phase.

A risk assessment of vapour phase H<sub>2</sub>S inhalation risks should be conducted in order to anticipate the most appropriate safety procedures, training, and personal protective equipment for situations that could involve storage tank headspaces, confined spaces, areas in the vicinity of tank venting pipes, storage containers for product residue, waste and waste water, as well as areas surrounding unintentional spills and releases.

For protecting personnel working in the vicinity of fuel storage tanks or vents, electronic alarms should be used that continuously monitor vapour phase H<sub>2</sub>S concentrations. When high vapour phase H<sub>2</sub>S concentrations are suspected or measured around a spilled product, additional or specialized personnel protection may be warranted, including restricting access to the spill area, using personal protective equipment, and ensuring the use of proper safety procedures.

Importantly, this report reinforces the need for safe handling procedures and appropriate personal protection when transferring or storing fuels that may contain H<sub>2</sub>S, rather than relying only on a measured H<sub>2</sub>S level in the liquid product.





## 1. BACKGROUND

The safe handling of petroleum cargoes and refined products that contain hydrogen sulphide ( $H_2S$ ) in the liquid phase is an important issue for the marine and inland fuel industries. Attention has refocused recently on  $H_2S$  due to revision of ISO 8217:2012 'Petroleum products — Fuels (class F) — Specifications of marine fuels' [1]. This specification for marine fuels limited the maximum content of  $H_2S$  in the liquid fuel to 2.00 mg  $H_2S$ /kg fuel (2.00 ppmw).

This report reviews issues associated with the presence of  $H_2S$  in residual marine fuels including:

- Sources of  $H_2S$  in petroleum products [4];
- Exposure levels to  $H_2S$  in the vapour phase and the effects of exposure [5,6];
- Relationship between  $H_2S$  in the liquid and vapour phases;
- Measurement methods for  $H_2S$  in the liquid and vapour phases;
- Interpretation of results and guidance on maximum  $H_2S$  levels; and
- General guidelines for the safe handling of liquid petroleum products that may contain  $H_2S$  [5].

Unlike residual marine fuels, marine distillate fuels do not normally contain  $H_2S$  at concentrations in the liquid phase that would result in safety concerns for fuel storage and handling. Under certain circumstances, however, higher  $H_2S$  levels can be present in the liquid phase of marine distillate fuels (e.g. when produced from sour crude oils without extensive hydroprocessing). The revised ISO 8217 marine fuel specification states that the liquid phase  $H_2S$  limit shall be measured by IP 570 [2] and the scope of this method now includes marine distillate fuels.

## 2. SOURCES OF HYDROGEN SULPHIDE

Hydrogen sulphide (H<sub>2</sub>S) occurs naturally in crude oils and the H<sub>2</sub>S concentration in the liquid phase can vary depending upon the origin of the crude. H<sub>2</sub>S can also be formed during the refining process from the conversion of sulphur-containing compounds in the crude oil by thermal processing or by catalytic cracking in the presence of hydrogen. Higher liquid phase H<sub>2</sub>S levels are typically found in fuel products produced by thermal or catalytic processes, such as hydrodesulphurisation, hydrocracking, and visbreaking.

Thus, the concentration of liquid-phase H<sub>2</sub>S that can be found in fuel products will depend upon the sulphur levels in the crude oil before processing and the type and severity of refinery processes used to produce the fuel product. In addition, hydrogen sulphide can be produced from sulphur-containing fuel products in storage by the action of anaerobic bacteria that can sometimes be found in the fuel supply and distribution system. Good housekeeping practices [7,8] can avoid these problems.

H<sub>2</sub>S will partition into the vapour phase from liquid fuel products that contain H<sub>2</sub>S, for example, from liquid fuels in storage tanks, product barges and customer tanks. H<sub>2</sub>S will also dissolve in water layers in tanks and barges that are in contact with the liquid fuel product. Heated surfaces (e.g., in-tank electrical heaters, steam coils, etc.) that are in direct contact with the liquid can also generate H<sub>2</sub>S from the conversion of sulphur-containing molecules in the liquid product by localised overheating. Importantly, this could happen after the fuel product has left the refinery, for example, in storage tanks at distribution terminals or at the customer's facility.

Hence, it is important that all parties involved in the manufacture, supply, distribution and use of residual fuels fully understand these effects and follow appropriate storage and handling procedures. It is also important that ship owners, operators and other parties maintain appropriate safety procedures, practices, and personnel training that are designed to protect the crew and others who could be exposed to H<sub>2</sub>S. Most importantly, a maximum liquid phase H<sub>2</sub>S specification in ISO 8217 [1] does not replace these safety requirements even though it is intended to limit the maximum H<sub>2</sub>S that can evolve from the liquid fuel into the vapour phase.

H<sub>2</sub>S, if present in the fuel product, will be present in the liquid and vapour phases, as well as in a water phase if one is present. In a closed storage vessel, H<sub>2</sub>S will partition from the liquid phase into the vapour phase until an equilibrium has been reached between the two phases. The equilibration time and the concentrations in each phase will depend upon a number of factors including:

- temperature of the liquid fuel;
- the fuel's chemical composition, including other contaminants and additives;
- the fuel's physical properties, particularly its viscosity;
- volume of fuel in the storage vessel (which governs the fuel volume relative to the head space volume);
- amount of applied heating to surfaces in contact with the liquid fuel;
- degree of liquid agitation;
- configuration of the tank, and, in particular, how the tank is vented;
- length of time the liquid fuel has been in storage;

- presence of water and a separate water phase; and
- ambient conditions (governing the amount of headspace purging/breathing).

In principle, H<sub>2</sub>S concentrations at equilibrium can be estimated from Raoult's Law for vapour pressures of multicomponent solutions. In practice, the confounding factors mentioned above make such estimates very difficult to do except in the simplest circumstances.

The H<sub>2</sub>S liquid to vapour ratio is therefore very difficult to predict. Available information suggests that this ratio for residual fuel oil can be in the range 1:50 to 1:100 in some instances, that is, 1 ppmw H<sub>2</sub>S in the liquid phase could produce between 50 to 100 ppmv H<sub>2</sub>S in the vapour phase. This is an approximation only and should be used with care as specific circumstances may produce H<sub>2</sub>S levels in the vapour phase that could be much higher. These estimates are based on published data [6,8] and on unpublished studies carried out by oil companies.

A 2010 study [10] by DNV Petroleum Services (DNVPS) compared the liquid phase H<sub>2</sub>S levels in 75 heavy fuel oil samples stored in bunker barge tanks against the vapour phase H<sub>2</sub>S levels in the tank's headspace. These samples represented 25 bunkerings and were analysed using the IP 570 test method recommended in ISO 8217.

The H<sub>2</sub>S concentration in the liquid fuels averaged 0.94 mg H<sub>2</sub>S /kg fuel (ppmw) with a range of 0.3 to 4 mg/kg (ppmw). Measurements showed that different fuel samples having the same liquid phase H<sub>2</sub>S level could result in vapour phase H<sub>2</sub>S levels that ranged from negligible amounts to more than 5 ppmv. The H<sub>2</sub>S levels in liquid samples from the tank were also consistently higher than those found in liquid samples taken at the ship's manifold and returned to an on-shore laboratory for analysis. The study showed that the vapour phase H<sub>2</sub>S concentration does not depend solely on the H<sub>2</sub>S concentration in the liquid fuel.

Although the H<sub>2</sub>S vapour/liquid/ ratios were lower than have been reported in previous studies [6,8], the authors of the DNVPS study concluded that the 2.00 mg H<sub>2</sub>S/kg fuel limit in ISO 8217 did not provide an adequate level of protection on its own against H<sub>2</sub>S in the vapour phase, even though the measured values were within occupational short-term exposure limits (see Section 3).

### 3. EFFECTS AND PROPERTIES OF H<sub>2</sub>S

At ambient temperatures, H<sub>2</sub>S is a highly toxic gas and the effects on exposed personnel depend on the H<sub>2</sub>S concentration and the duration of exposure. At very low concentrations, the gas has the characteristic smell of rotten eggs. However, at moderate concentrations, H<sub>2</sub>S causes sensory irritation, a temporary loss of sensitivity to H<sub>2</sub>S smell (transitory olfactory fatigue), headaches and dizziness. At high concentrations above 300 ppmv, H<sub>2</sub>S may cause unconsciousness and death. Exposure to H<sub>2</sub>S concentrations above 700 ppmv is immediately fatal.

The following table summarises the effects of exposure at different concentrations.

**Table 1** Effects of exposure to different vapour phase concentrations of H<sub>2</sub>S [11,12,13]

H <sub>2</sub> S concentration (ppmv)	Physiological Effects
0.0005 - 0.5	First detectable by smell (disagreeable odour of rotten eggs)
1 - 5	Limit for 8 hours working May cause some nausea
5 - 10	Short-term exposure limit (STEL) May cause nausea and eye lacrimation after prolonged exposure in sensitive individuals
50 – 100	Respiratory tract and eye irritation after 1 hour Headaches and dizziness. Longer exposures to concentrations up to 100 ppmv result in a gradual increase in the severity of these symptoms. Unconsciousness leading to death may occur after 4 – 48 hours of exposure
100	Loss of sense of smell. Olfactory paralysis occurs after 3 to 15 minutes exposure to 100 ppmv
200	Exposures of over 30 minutes may cause delayed chemical pneumonitis (lung oedema)
350	Unconsciousness leading to death may occur after 30 minutes exposure
>500	Rapid ('knock down') unconsciousness and death. Causes seizures, loss of control of bladder and bowels. Breathing will stop and death will result if victim is not rescued and resuscitated promptly.
700+	Immediately fatal

Long-term Occupational Exposure Limits (OELs) typically represent the time-weighted average (TWA) exposure concentration of a toxic substance permitted over an 8-hour working day and a 40-hour working week. They represent a concentration to which most workers may be repeatedly exposed, day after day, without significant adverse health effects. In the case of hydrogen sulphide, the limit is primarily based on avoiding transient sensory irritation in the eyes, nose, and throat.

Such limits are based on professional assessments of the best available information at a particular point in time and are regularly updated by health regulatory authorities. OELs are intended to protect most of the working population from adverse health effects but some exceptions may occur with unusually sensitive individuals. For some substances, as is the case for H<sub>2</sub>S, brief exposures to high vapour concentrations may cause localised irritation that require establishing short-term exposure limits (STELs). STELs typically represent a 15-minute TWA concentration that should not be exceeded.

### 3.1. OCCUPATIONAL EXPOSURE LIMITS FOR H<sub>2</sub>S IN THE VAPOUR PHASE

Occupational limits for vapour phase H<sub>2</sub>S have been revised and lowered in many different countries and regions:

- The European Commission's Scientific Committee on Occupational Exposure Limits (SCOEL) recommends a 5 ppmv (7 mg/m<sup>3</sup>) TWA (8-hour), with a 10 ppmv (14 mg/m<sup>3</sup>) STEL (15 minutes) [14];
- In the Netherlands, the current Maximally Allowed Concentration (MAC) is 1.6 ppmv (or 2.3 mg/m<sup>3</sup>) [13];
- In the United Kingdom, 5 ppmv (7 mg/m<sup>3</sup>) is recommended for the derived and OEL limits (8 hours TWA) with a 10 ppmv (14 mg/m<sup>3</sup>) STEL [11];
- In Germany, 5 ppmv (7.1 mg/m<sup>3</sup>) is recommended by the MAK Commission [21];
- ACGIH® has recommended 1 ppmv as the Threshold Limit Value (TLV) with a 5 ppmv (or 7 mg/m<sup>3</sup>) STEL [12]. This TLV has also been legally adopted in several European countries.

The prevailing limit values should be carefully reviewed to ensure compliance before storing or handling products containing liquid or vapour phase H<sub>2</sub>S or that have the potential to evolve H<sub>2</sub>S under storage conditions.

## 4. MEASUREMENTS OF H<sub>2</sub>S

Test methods have been developed by the Energy Institute (EI), ASTM, and others to measure H<sub>2</sub>S in the liquid or vapour phase. In-house methods have also been developed by some oil companies, inspection services, and other companies.

### 4.1. MEASUREMENTS OF H<sub>2</sub>S IN THE LIQUID PHASE

Measurements of H<sub>2</sub>S in the liquid phase report the amount of H<sub>2</sub>S dissolved in the liquid fuel. These liquid phase values indicate the potential levels of H<sub>2</sub>S that could be generated in the vapour phase if all of the liquid phase H<sub>2</sub>S were to be released to the vapour phase. As indicated above, however, the liquid/vapour ratio can be very variable and liquid phase measurements provide only an approximate indication of potential vapour phase H<sub>2</sub>S levels.

There are a number of different methods for measuring the concentration of H<sub>2</sub>S in the liquid phase. A comprehensive study was undertaken by the EI in the late 1980's, which concluded that many methods could give inaccurate results. To overcome problems with mostly in-house laboratory methods, the EI developed and published method IP 399 [3], titled 'Determination of hydrogen sulphide in fuel oils'.

IP 399 is a "wet" chemical procedure requiring the use of hazardous chemicals and well-trained and competent laboratory technicians. The procedure is time-consuming and too complex to be used routinely. Changes to the test method have taken place over time, primarily a change of one of the key chemical reagents (cadmium sulphate was replaced by zinc acetate). It is believed that the published precision from the most recent round robin exercise for IP 399 is no longer valid when the zinc acetate reagent is used.

To overcome perceived weaknesses in the IP 399 method, the EI developed IP 570, 'Determination of Hydrogen Sulphide in Fuel Oils - Rapid liquid phase extraction method'. In this method, a weighed liquid sample is placed in a heated test vessel, containing a base oil diluent. Air is bubbled through the heated liquid to extract the H<sub>2</sub>S gas which is then passed over a selective detector to measure the H<sub>2</sub>S content in the air. The amount of H<sub>2</sub>S in the liquid phase is then calculated in mg H<sub>2</sub>S/kg fuel.

The IP 570 test was originally only applicable to marine residual fuels, however, additional testing coordinated by the EI has seen the scope of the test method extended to include marine distillate fuels.

Interference problems with the IP 570 measurement have been noted by some users when low boiling point materials, such as ethyl and methyl mercaptans and alkyl sulphides, are also present in the fuel. To address this problem, the equipment manufacturer has developed a cold trap called a Vapour Phase Processor (VPP). The VPP traps the interfering molecules in a cold trap at -20°C, separating the H<sub>2</sub>S measured by the detector from the other contaminants. Interfering molecules are likely to lead to higher measured values of H<sub>2</sub>S in the liquid phase.

The EI recently completed an inter-laboratory study to establish the precision of the IP 570 test method using the VPP. The 2012 version of IP 570 now includes Procedure A (with the VPP) and Procedure B (without the VPP). Since many marine fuels will not contain interfering molecules, it is not always necessary to follow Procedure A when testing samples and Procedure B will be sufficient. However, if it is suspected that interfering molecules may be present, then it is recommended that

Procedure A is used. The newest edition of ISO 8217 includes Procedure A as the reference test method.

CONCAWE recommends that IP 570 is used both as the definitive referee method (Procedure A) and for routine sample testing (Procedure A or B).

#### **4.2. SAMPLING AND HANDLING CONSIDERATIONS**

To ensure reliable and consistent liquid phase H<sub>2</sub>S measurements, great care must be taken during sampling and subsequent handling and in the selection of sample containers. The following sampling and handling requirements for residual fuel oil samples are included in IP 570 [2]:

- It is recommended that only epoxy-lined cans or dark brown borosilicate glass bottles with impervious gas-tight closures of a minimum volume of 500 ml should be used for collecting liquid fuel samples for testing;
- These cans or bottles should be completely filled to approximately 95% volume capacity and should then be immediately sealed;
- Sample containers should be taken to the test laboratory as soon as possible after sampling and should be immediately tested if possible. If samples are not tested immediately, they should be stored in a cool place such as a refrigerator and analysed within no more than 3 days.
- IP 570 shall be the first test performed on the sample as any additional handling can lead to loss of H<sub>2</sub>S and low results.

IP 570 further specifies that samples must be drawn in accordance with IP 475 (ISO 3170) [15]. This standard describes various sampling methods either for taking “grab” samples from various positions within a tank’s fuel volume (usually top, middle and bottom) or from a pipeline, or for taking “running” samples from a vertical column through the liquid. These methods are very different from the continuous drip sampling method [16] that is generally used for drawing a representative sample during a marine bunker delivery.

Most samples of marine fuels are drawn in accordance with sampling procedures developed by the International Maritime Organisation (IMO, [16]) for the purpose of determining the sulphur content in the fuel. These guidelines specify that the fuel sample should be obtained at the receiving ship’s inlet bunker manifold and drawn continuously throughout the bunker delivery period. This is done using a drip sampler where the sample literally drips into a closed sample container throughout the bunkering operation. The drip sample is subsequently split into a number of smaller samples, some of which are retained by the fuel supplier while others are taken by the ship operator. In order to ensure that the fuel sample is homogenous before it is split into smaller samples, the IMO guideline specifies that the sample should be thoroughly agitated before splitting.

Samples obtained by the continuous-drip method could lead to an under estimation of the amount of H<sub>2</sub>S in the delivered fuel for two reasons: (1) loss of H<sub>2</sub>S from the liquid fuel due to the high surface area liquid/gas interface that is associated with the continuous-drip sampling method and the subsequent sample agitation/splitting process and (2) loss of H<sub>2</sub>S due to the materials that are typically used when collecting such samples. Care should be taken to ensure that the integrity of the sample is maintained and that the possible loss of H<sub>2</sub>S is kept to a minimum. At present, no data are available to quantify typical levels for these losses. Where samples are drawn in

a manner that does not minimise vapour loss (e.g. continuous drip sampling), separate samples should be drawn for H<sub>2</sub>S determination.

Therefore, H<sub>2</sub>S results obtained on a liquid bunker sample collected by the continuous drip method could lead to measured H<sub>2</sub>S concentrations that are too low due to vapour loss, which could lead to a false sense of security. Liquid fuel samples must be specifically taken for the determination of liquid phase H<sub>2</sub>S in accordance with the guidance provided above.

#### **4.3. MEASUREMENTS OF H<sub>2</sub>S IN THE VAPOUR PHASE**

Vapour phase H<sub>2</sub>S measurements indicate the H<sub>2</sub>S level at a particular location and at a particular point in time. Such measurements do not determine the potential levels of H<sub>2</sub>S that could be generated if most of the H<sub>2</sub>S in the liquid phase evolved into the vapour phase.

ASTM D5705 [17] ('Standard test method for measurement of hydrogen sulphide in the vapour phase above residual fuel oils') measures the levels of vapour phase H<sub>2</sub>S under prescribed test conditions. Vapour phase measurements are reported as parts per million on a volume basis (denoted "ppmv"). Although ASTM D5705 is described as a field test method, most field measurements use a simplified version of this method in which a fixed volume of vapour is drawn through a stain-detector tube. A stain-detector tube is one that contains a material that changes colour upon exposure to H<sub>2</sub>S vapour. Simplified methods such as this are prone to errors and are very dependent upon the location of the sampling point, in particular on its proximity to the source of H<sub>2</sub>S.

Electronic monitoring devices are also available as an alternative to stain-detector tubes but the results from these devices are very dependent upon the location of the point of measurement. However, these devices can and should be used to alert personnel to H<sub>2</sub>S vapours that may be emanating from open tank hatches and outlets of tank vents.

As stated earlier, the concentration of H<sub>2</sub>S in the headspace of a tank will depend on many factors and not just the total amount of H<sub>2</sub>S in the liquid phase and on the partitioning between the liquid and vapour phases (see Section 2). Importantly, a measurement that indicates a low concentration of H<sub>2</sub>S does not necessarily mean that this will be the case in the future. Depending upon changing conditions in the tank, H<sub>2</sub>S vapour could evolve from the liquid into the vapour space at a later time, especially if the amount of product in the tank has changed. Therefore, opening a tank and taking a headspace tank measurement can provide misleading results. In some circumstances, the headspace may indicate that there is no H<sub>2</sub>S in the vapour space while the liquid fuel may contain a significant concentration of H<sub>2</sub>S.



## 5. ISO 8217 GUIDANCE ON H<sub>2</sub>S LEVELS IN THE LIQUID PHASE

The marine fuel specification (ISO 8217) now includes a maximum H<sub>2</sub>S limit in the liquid fuel, as measured by IP 570. It should be noted that inland fuel oil and commercial blend component specifications do not typically stipulate a maximum H<sub>2</sub>S limit in the liquid phase but it is recommended that similar safety precautions should be observed.

The inclusion of this H<sub>2</sub>S limit in ISO 8217 can be expected to reduce the potential maximum H<sub>2</sub>S vapour that can volatilise from the fuel. However, as described earlier, low H<sub>2</sub>S results in the vapour phase can be obtained if the sampling requirements specified in IP 570 are not rigorously followed. Similarly, low H<sub>2</sub>S results can also be obtained on tank headspace samples if the liquid in the tank is of high viscosity and has not been agitated. In both of these cases, a false sense of personnel safety can occur.

To ensure greater safety to personnel, it is therefore critical that ship owners, operators and other parties who may be exposed to H<sub>2</sub>S (e.g. those involved in sampling or gauging tanks via open hatches) are properly trained on H<sub>2</sub>S hazards and that they routinely operate within the established safe procedures. These procedures should include the use of personal H<sub>2</sub>S alarms and, if necessary, other appropriate personal protective equipment (PPE). Many good videos and on-line training modules are now available (see [18] as an example). Local health and safety specialists who are knowledgeable in H<sub>2</sub>S hazards should also be consulted.

The oil industry regularly handles cargoes (e.g. some crude oils and high-sulphur process streams) containing much higher H<sub>2</sub>S levels than are typically found in marine fuels. These cargoes are carried by specialized ship operators who ensure that their crews through regular training are fully aware of the potential risks and the importance of prescribed handling procedures. These procedures have proven to be sufficient to provide a very high degree of personnel protection without the need for additional controls on the H<sub>2</sub>S concentration in the cargo itself.

## 6. PRODUCT HANDLING AND SAFETY PRECAUTIONS

Since residual fuel oils may contain H<sub>2</sub>S, normal operations of loading/unloading and tank sampling and gauging should take the potential presence of H<sub>2</sub>S into account. It is therefore recommended that all facilities dealing with residual fuel oil have an H<sub>2</sub>S safety awareness programme in place and that all employees dealing with product handling are well-trained. Details of such a programme will be location specific, but the following elements should at least be considered:

- H<sub>2</sub>S awareness and training plan;
- Permit to work system and 'toolbox' meeting prior to starting work;
- Confined space entry procedures and training;
- H<sub>2</sub>S detection systems, including personal alarms;
- Emergency evacuation and operational procedures;
- Personal protective equipment including supplied air respirators, eyewear, and flame-retardant clothing;
- Specific operating instructions for cargos with high liquid phase H<sub>2</sub>S concentrations; and
- Near miss and incident reporting, with follow-up plans [19].

Routine operations in open or well-ventilated spaces are unlikely to present serious hazards when H<sub>2</sub>S concentrations in the liquid fuel are low (that is, up to 2.00 mg H<sub>2</sub>S/kg fuel). However, inside tanks and in the immediate proximity of open tank hatches and tank vents, H<sub>2</sub>S levels could exceed both short-term and long-term OELs although vapour-phase H<sub>2</sub>S levels in these locations are not likely to approach the levels at which sudden and serious health effects will occur. Nonetheless, personnel precautions and training should always be enforced even when the liquid-phase H<sub>2</sub>S concentrations are known to be low.

Because H<sub>2</sub>S is denser than air, it should also be recognised that higher concentrations of H<sub>2</sub>S may be found in low points, such as in confined spaces including sumps and pits that are not well ventilated. It is therefore important that proper procedures and training are in place for all personnel who are required to work near open tank hatches (e.g. when gauging tanks) or when working for prolonged periods close to tank vent outlets [20]. This includes the use of personal H<sub>2</sub>S alarms, supplied air respirators, and other PPE (where required), when other safety management options cannot guarantee personnel safety.

During some occasional or non-routine operations, such as during inspections and maintenance, personnel entry into tanks (even when the tanks are nominally empty) presents many very serious hazards in addition to those due to H<sub>2</sub>S. Rigorous safety procedures are required for any occasions when personnel must enter enclosed work spaces, such as storage tanks.

When dangerously high amounts of H<sub>2</sub>S are suspected or measured around a spilled product, additional or special actions may be warranted, including restricting access to the spill area, using special PPE, such as a self-contained breathing apparatus, and the use of proper evacuation procedures. A specific assessment of inhalation risks due to the presence of H<sub>2</sub>S in the vapour phase of storage tank headspaces, confined spaces, and product residue, waste and waste water containers and in the area surrounding unintentional releases should be made in order to determine the

most appropriate personnel protection and control measures for the given circumstances. Proper procedures and personnel training based on facility assessments are also important and should be regularly reinforced.

It is beyond the scope of this document to cover these considerations in detail, however, and specialist advice should be sought before encountering these situations.

## 7. ACRONYMS

ACGIH®	American Conference of Governmental Industrial Hygienists®
ASTM (International)	American Society for Testing Materials (original name)
DNVPS	DNV Petroleum Services
EI	Energy Institute (formerly called the Institute of Petroleum)
H <sub>2</sub> S	Hydrogen Sulphide
IMO	International Maritime Organisation
IP	Institute of Petroleum
ISO	International Standards Organisation
MAC	Maximally Allowed Concentration
OEL	Occupational Exposure Level
PPE	Personal Protective Equipment
ppmw	parts per million (weight basis)
ppmv	parts per million (volume basis)
SCOEL	Scientific Committee on Occupational Exposure Limits (of the European Commission)
STEL	Short-term Exposure Limit
TLV	Threshold Limit Value
TWA	Time Weighted Average
VPP	Vapour Phase Processor

## 8. ACKNOWLEDGMENTS

CONCAWE's Marine Fuels Ad Hoc Group would like to thank the following individuals for their contributions to this document:

- Harry Read, Energy Institute, United Kingdom
- Adrian Daniels, BP Marine
- David Morgott, LyondellBasell
- Gary Minsavage and Arlean Rohde, Health Science Executives, CONCAWE
- Klaas den Haan, Safety Science Executive, CONCAWE
- Pete Roberts, Air Quality Science Executive, CONCAWE

---

## 9. REFERENCES

1. ISO (2012) Petroleum products — Fuels (class F) — Specifications of marine fuels. International Standard ISO 8217:2010. Technical Corrigendum 1. Geneva: International Organization for Standardization
2. IP (2012) Determination of hydrogen sulphide in fuel oils – Rapid liquid phase extraction method. IP Standard Method 570. London: Energy Institute
3. IP (2010) Determination of hydrogen sulphide in fuel oils. IP Standard Method 399. London: Energy Institute
4. Cush, M. (2009) Hydrogen Sulphide - General Information (Version 1). London: Health Protection Agency
5. Cush, M. (2011) HPA Compendium of Chemical Hazards - Hydrogen Sulphide (Version 2). London: Health Protection Agency
6. CAPP (2003) Occupational Health and Safety of Hydrogen Sulphide (H<sub>2</sub>S). Calgary: Canadian Association of Petroleum Producers
7. CEN (2007) Petroleum products - guide for good housekeeping. Automotive diesel fuels. CEN/TR 15367-1. Brussels: Comité Européen de Normalisation
8. CEN (2009) Petroleum products - guide for good housekeeping. Prevention of cross contamination. CEN/TR 15367-3. Brussels: Comité Européen de Normalisation
9. Slack, D.J. (1988) Hydrogen sulphide in residual fuel oil and storage tank vapor space. *Am Ind Hyg Assoc J* 49, 4, 205-206
10. DNV (2010) DNV Petroleum Services field study probes 2 mg/kg H<sub>2</sub>S maximum limit in ISO 8217:2010 marine fuel specification. Oslo: DNV Petroleum Services [http://www.dnv.com/news\\_events/news/2010/dnvpetroleumservicesfieldstudypobes2mgkgH2Smaximumlimitiniso82172010marinefuelspecification.asp](http://www.dnv.com/news_events/news/2010/dnvpetroleumservicesfieldstudypobes2mgkgH2Smaximumlimitiniso82172010marinefuelspecification.asp)
11. Cush, M. (2011) Hydrogen Sulphide - Toxicological Overview (Version 2). London: Health Protection Agency
12. ACGIH® (2010). Hydrogen Sulfide: TLV® Chemical Substances 7<sup>th</sup> Edition Documentation. Cincinnati: American Conference of Governmental Industrial Hygienists
13. DECOS (2006) Hydrogen sulphide - Health-based recommended occupational exposure limit in the Netherlands. No. 2006/07OSH. The Hague: Dutch Expert Committee on Occupational Standards
14. SCOEL (2007) Recommendation from the Scientific Committee on Occupational Exposure Limits for Hydrogen Sulphide. SCOEL/SUM/124. Luxembourg: Office for Official Publications of the European Communities
15. IP (2005) Petroleum liquids – Manual sampling (ISO 3170:2004). IP Standard Method 475. London: Energy Institute

16. IMO (2002) Guidelines for the sampling of fuel oil for determination of compliance with Annex VI of Marpol 73/78. MEPC 47/20. Annex 2. Resolution MEPC.96(47). London: International Maritime Organisation
17. ASTM (2012) Standard test method for measurement of hydrogen sulfide in the vapor phase above residual fuel oils. ASTM D5705. Philadelphia PA: American Society for Testing and Materials
18. OSHA (2012) General Safety and Health >> Hydrogen Sulfide Gas. Washington DC: Occupational Safety & Health Administration [http://www.osha.gov/SLTC/etools/oilandgas/general\\_safety/h2s\\_monitoring.html](http://www.osha.gov/SLTC/etools/oilandgas/general_safety/h2s_monitoring.html)
19. Bull, S (2008) Hydrogen sulphide - Incident management (Version 1). London: Health Protection Agency
20. EI (2011) Hydrocarbon management - HM 50 Guidelines for the cleaning of tanks and lines for marine tank vessels carrying petroleum and refined products. London: Energy Institute
21. MAK (2012) Substance Overview for Hydrogen Sulfide. The MAK Collection for Occupational Health and Safety. 1. Weinheim: Wiley-VCH Verlag





CONCAWE  
Boulevard du Souverain 165  
B-1160 Brussels  
Belgium

Tel: +32-2-566 91 60  
Fax: +32-2-566 91 81  
e-mail: [info@concawe.org](mailto:info@concawe.org)  
website: <http://www.concawe.org>

ISBN 978-2-87567-022-9



9 782875 670229 >